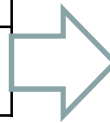


ME265: Thermal Engineering & Heat Transfer

Chapters
1. Energy Scenario
2. Thermodynamics
3. Mechanical Devices & Systems
4. Heat Transfer



4.1 Introduction	
4.2 Conduction	4.2.1 Conduction Equations 4.2.2 Boundary & Initial conditions 4.2.3 Steady Heat Conduction 4.2.4 Transient Heat Conduction
4.3 Convection	
4.4 Radiation	
4.5 Heat Exchanger	

4.2.3	Steady Heat Conduction	
	4.2.3.1	Solutions to 1D-SS HC problems
	4.2.3.2	Thermal resistances
	4.2.3.3	R-values of Insulation
	4.2.3.4	Critical thickness of insulation
	4.2.3.5	Thermal analysis of fins

4.2.3 Steady Heat Conduction

4.2.3.5 Thermal Analysis of fins

Fins are extended surfaces to enhance the rate of heat transfer.

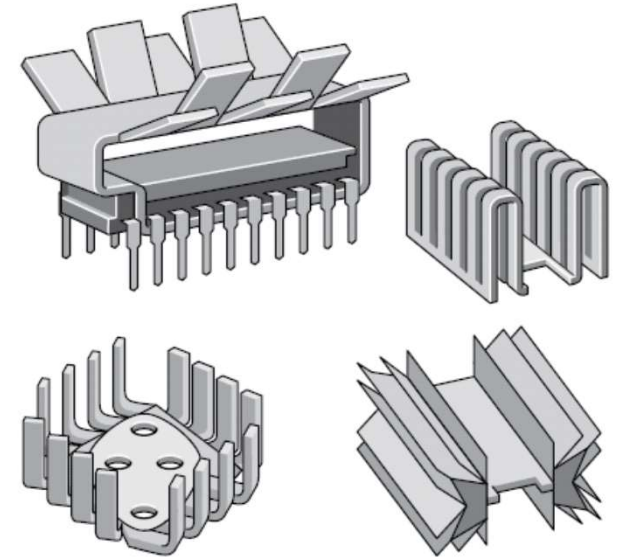
We know from Newton's law cooling

$$\dot{Q} = h A_s (T_s - T_\infty)$$

- ✓ Two ways to increase the heat transfer:
 - increasing the heat transfer coefficient h
 - increase the surface area A_s

- ✓ *The increase in h requires the change of surrounding fluid and its condition, but this approach may not be always practically feasible.*

- ✓ *The increase in A_s can easily be done by using of the **extended surfaces** called **fins***



4.2.3 Steady Heat Conduction

4.2.3.5 Thermal analysis of fins: **Fin Equation**

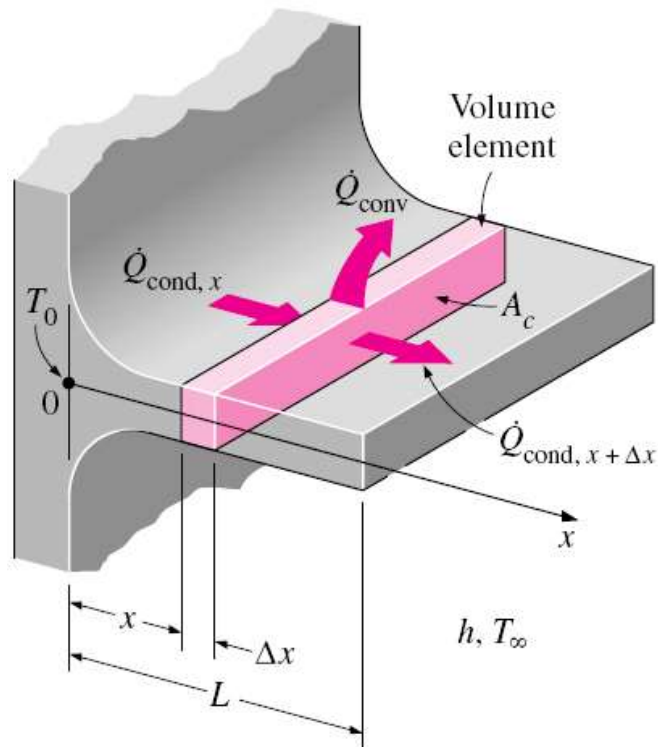


Fig. 2.1: A schematic of fin for Thermal Analysis

Under steady conditions, the energy balance on this volume element can be expressed as follows:

$$\left(\begin{array}{l} \text{Rate of heat} \\ \text{conduction into} \\ \text{the element at } x \end{array} \right) = \left(\begin{array}{l} \text{Rate of } \textit{heat} \\ \text{conduction from the} \\ \text{element at } x+\Delta x \end{array} \right) + \left(\begin{array}{l} \text{Rate of heat} \\ \text{convection from} \\ \text{the element} \end{array} \right)$$

$$\dot{Q}_{cond,x} = \dot{Q}_{cond,x+\Delta x} + \dot{Q}_{conv} \dots \dots \textbf{(2.3.1)}$$

By neglecting radiation effect

4.2.3 Steady Heat Conduction

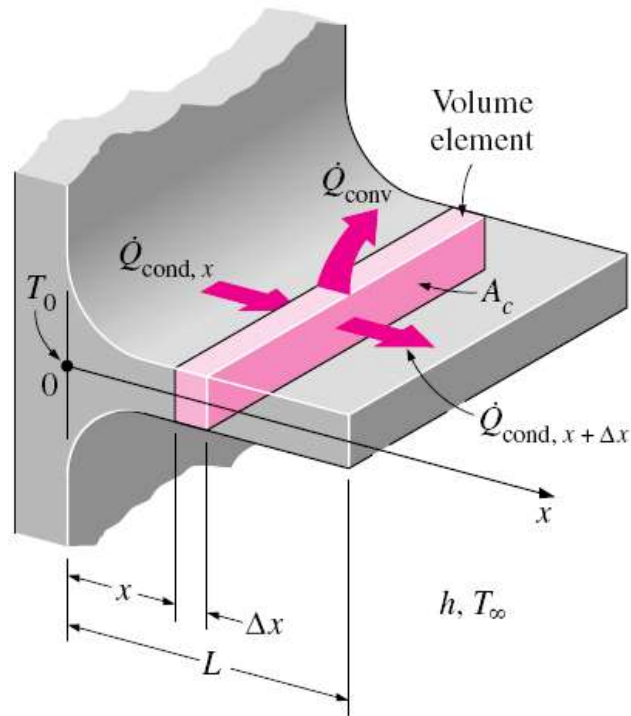


Fig. 2.1: A schematic of fin for Thermal Analysis

$$\frac{d^2\theta}{dx^2} - m^2\theta = 0 \quad \dots \dots (2.3.4)$$

$$\text{Where, } m^2 = \frac{hp}{kA_c}$$

This is the governing equation of fin. It is a linear, homogeneous, second-order differential equation with constant coefficients.

Therefore, the general solution is as follows:

$$\theta(x) = C_1 e^{mx} + C_2 e^{-mx} \quad \dots \dots (2.3.5)$$

C_1 and C_2 are arbitrary constants and are determined from the BCs.

4.2.3 Steady Heat Conduction

4.2.3.5 Thermal analysis of fins: Fin BCs

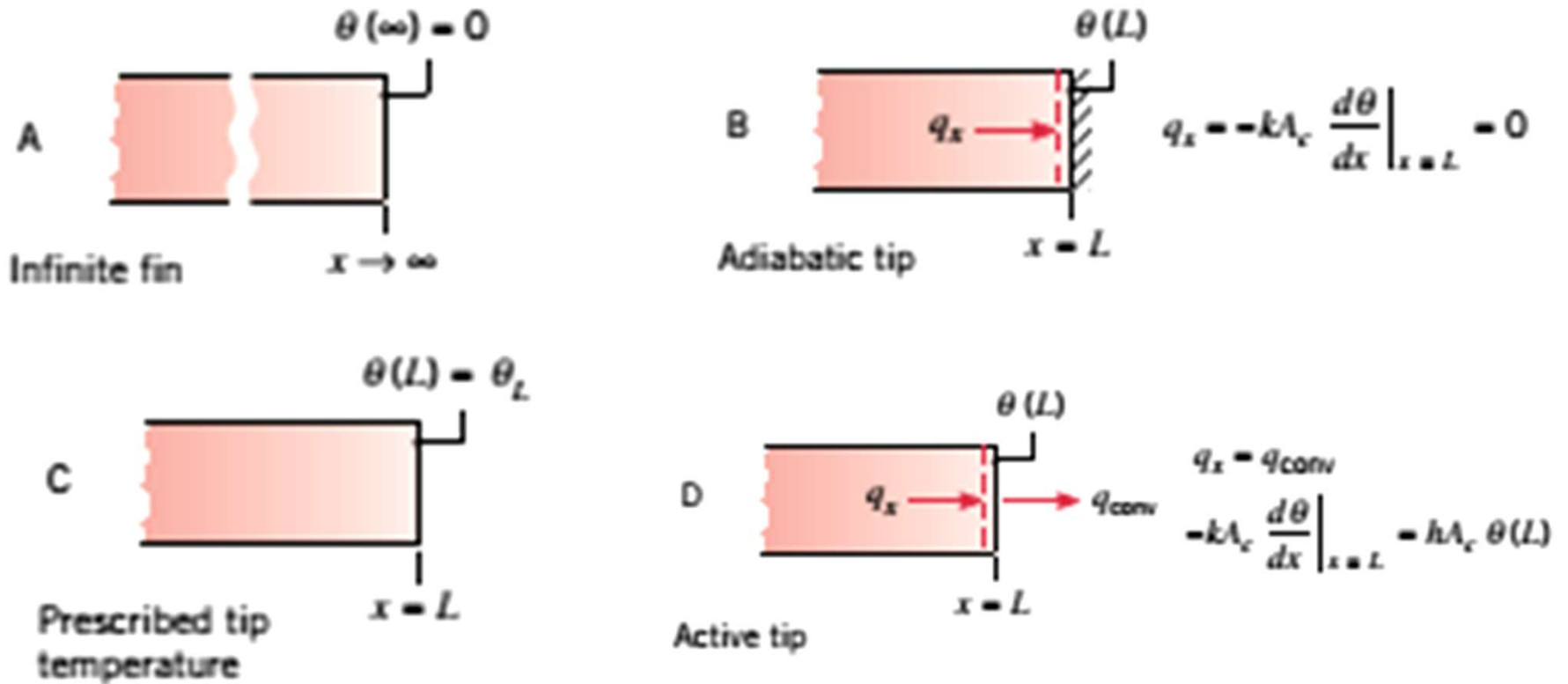


Fig. 2.2: Fin Boundary Conditions

$$\theta_b = T_b - T_\infty; \quad \theta_L = T_L - T_\infty$$

$$m = \sqrt{\frac{hp}{kA_c}} \dots \text{called fin parameter}$$

dimension: $\mathbf{m^{-1}}$

4.2.3 Steady Heat Conduction

4.2.3.5 Thermal analysis of fins: Fin BCs

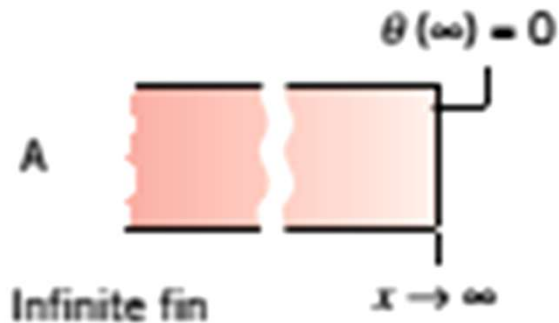


Fig. 2.2(a): Fin with BC—Case A

$$\theta(x) = C_1 e^{mx} + C_2 e^{-mx} \quad \dots \dots (2.3.5)$$

C_1 and C_2 are arbitrary constants and are determined from the BCs.

$$m = \sqrt{\frac{hp}{kA_c}} \quad \dots \dots \text{called fin parameter}$$

At $x=0$,

$$\theta(0) = \theta_b = C_1 + C_2$$

At $x=L \rightarrow \infty$,

$$\theta(L) = C_1 e^{mL} + C_2 e^{-mL} = 0$$

Therefore, $C_1 = 0$ and $\theta_b = C_2$

The temperature distribution:

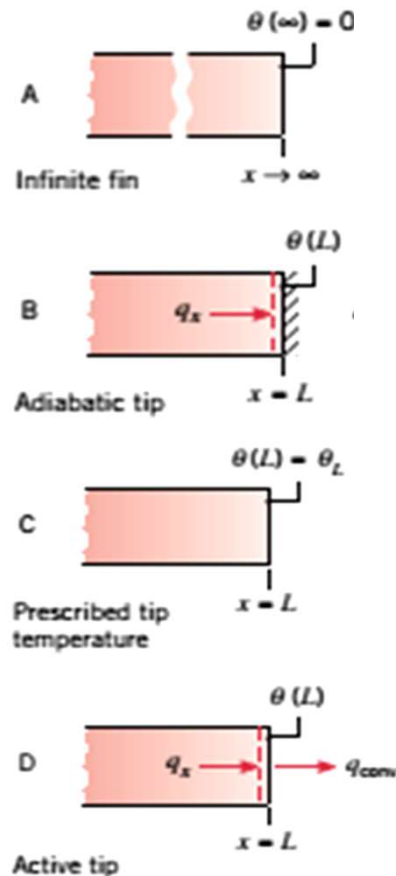
$$\frac{T(x) - T_\infty}{T_b - T_\infty} = e^{-mx} = e^{-x\sqrt{hp/kA_c}} \quad \dots \dots (2.3.6)$$

The rate of heat transfer:

$$\dot{Q} = -kA_c \left. \frac{dT}{dx} \right|_{x=0} = \sqrt{hp k A_c} (T_b - T_\infty) \quad \dots \dots (2.3.7)$$

4.2.3 Steady Heat Conduction

4.2.3.5 Thermal Analysis of fins: Summary for uniform c/s fin



Case	Temperature Distribution θ/θ_b	Rate of heat transfer \dot{Q}_f
A	e^{-mx}	$M = \sqrt{hp k A_c} \theta_b$
B	$\frac{\cosh m(L-x)}{\cosh mL}$	$M \tanh mL$
C	$\frac{\left(\frac{\theta_L}{\theta_b}\right) \sinh mx + \sinh m(L-x)}{\sinh mL}$	$M \frac{\cosh mL - \left(\frac{\theta_L}{\theta_b}\right)}{\sinh mL}$
D	$\frac{\cosh m(L-x) + \left(\frac{h}{mk}\right) \sinh m(L-x)}{\cosh mL + \left(\frac{h}{mL}\right) \sinh mL}$	$M \frac{\sinh mL + \left(\frac{h}{mk}\right) \cosh mL}{\cosh mL + \left(\frac{h}{mL}\right) \sinh mL}$

$$\theta = (T - T_\infty); \quad \theta_b = T_b - T_\infty; \quad \theta_L = T_L - T_\infty$$

$$m = \sqrt{\frac{hp}{kA_c}} \dots \dots \text{called fin parameter}$$

4.2.3.5 Analysis of Fins

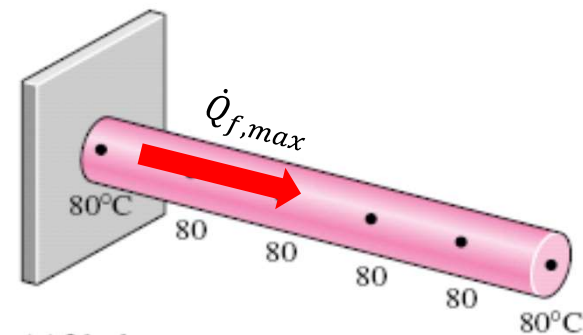
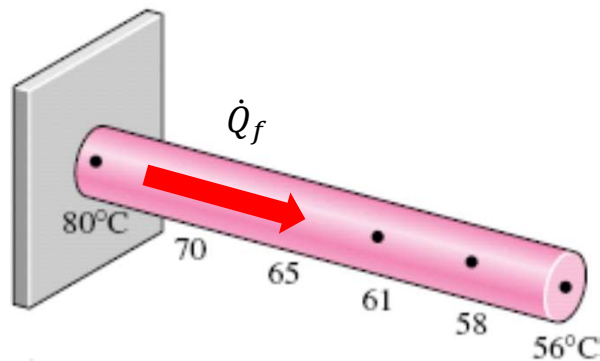
□ Performance parameters

- Fin Efficiency, η_f
- Fin Effectiveness, ε_f

4.2.3.5 Analysis of Fins

□ Performance parameters: Fin Efficiency, η_f

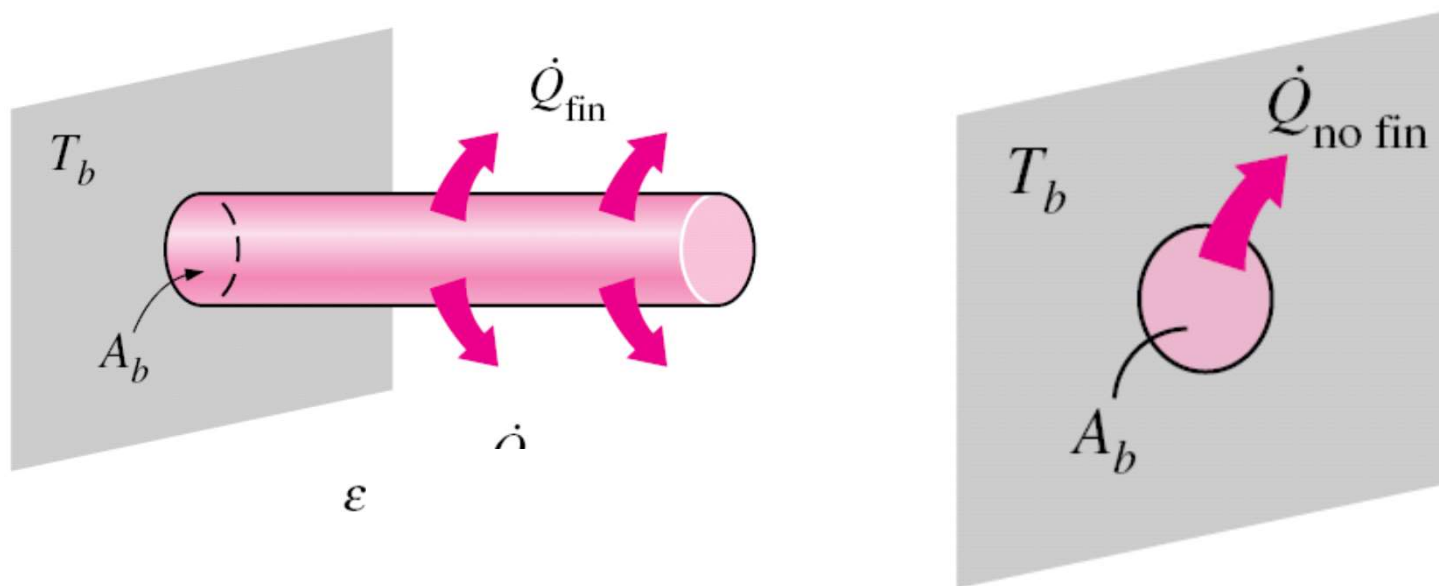
$$\eta_f = \frac{\text{Rate of heat transfer with fin}}{\text{Rate of heat transfer if entire fin surface were at base temperature}} = \frac{\dot{Q}_f}{\dot{Q}_{f,max}}$$



4.2.3.5 Analysis of Fins

□ Performance parameters: Fin Effectiveness, ϵ_f

$$\epsilon_f = \frac{\text{Rate of heat Transfer with fin}}{\text{Rate of heat transfer without fin}} = \frac{\dot{Q}_{fin}}{\dot{Q}_{no\ fin}}$$



Use of fin is not justified unless, $\epsilon_f \geq 2$

4.2.3.5 Analysis of Fins

□ Performance parameters

Fin efficiency and Fin effectiveness are related as follows:

$$\varepsilon_{\text{fin}} = \frac{\dot{Q}_{\text{fin}}}{\dot{Q}_{\text{no fin}}} = \frac{\dot{Q}_{\text{fin}}}{hA_b (T_b - T_\infty)} = \frac{\eta_{\text{fin}} hA_{\text{fin}} (T_b - T_\infty)}{hA_b (T_b - T_\infty)} = \frac{A_{\text{fin}}}{A_b} \eta_{\text{fin}}$$

4.2.3.5 Analysis of Fins

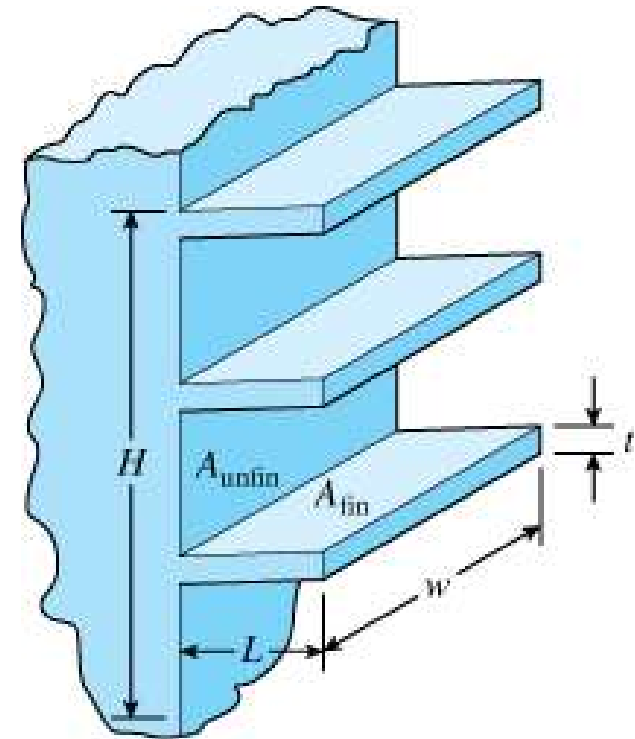
□ Performance parameters

Overall fin effectiveness:

$$\varepsilon_{fin,overall} = \frac{\dot{Q}_{fin}}{\dot{Q}_{no\ fin}}$$

$$\varepsilon_{fin,overall} = \frac{h(A_{unfin} + \eta_{fin}A_{fin})(T_b - T_\infty)}{hA_{no,fin}(T_b - T_\infty)}$$

$$\varepsilon_{fin,overall} = \frac{A_{unfin} + \eta_{fin}A_{fin}}{A_{no,fin}}$$



$$\begin{aligned} A_{no\ fin} &= w \times H \\ A_{unfin} &= w \times H - 3 \times (t \times w) \\ A_{fin} &= 2 \times L \times w + t \times w \\ &\cong 2 \times L \times w \text{ (one fin)} \end{aligned}$$

4.2.3.5 Analysis of Fins

□ Design consideration

$$\epsilon_{\text{long fin}} = \frac{\dot{Q}_{\text{fin}}}{\dot{Q}_{\text{no fin}}} = \frac{\sqrt{hpkA_c} (T_b - T_\infty)}{hA_b (T_b - T_\infty)} = \sqrt{\frac{kp}{hA_c}}$$

- The **thermal conductivity** k of the fin material should be as **high** as possible.
- The ratio p/A_c should be as **high** as possible.
- The use of fins is *most effective* in applications involving a **low** h



- ✓ The use of fins is more easily justified when the medium is a **gas** instead of a **liquid**
and
- ✓ the heat transfer is by **natural convection** instead of by **forced convection**.

4.2.3.5 Analysis of Fins

EP#2.6 Preventing circuit board from overheating

(Cengel et al Example 3-13)

A 15-cm x 20-cm integrated circuit board is to be cooled by attaching 4-cm-long aluminum ($k=237$ W/m.K) fins on one side as shown in the figure. Each fin has a 2-mm x 2-mm square cross-section. The ambient temperature is 25°C and the convection heat transfer coefficient on fin surface is 20 W/m².K. To prevent the circuit board from overheating, the upper surface of the board needs to be at 80°C or cooler. Determine the number of fins with overall effectiveness of 3.

